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Thermodynamics

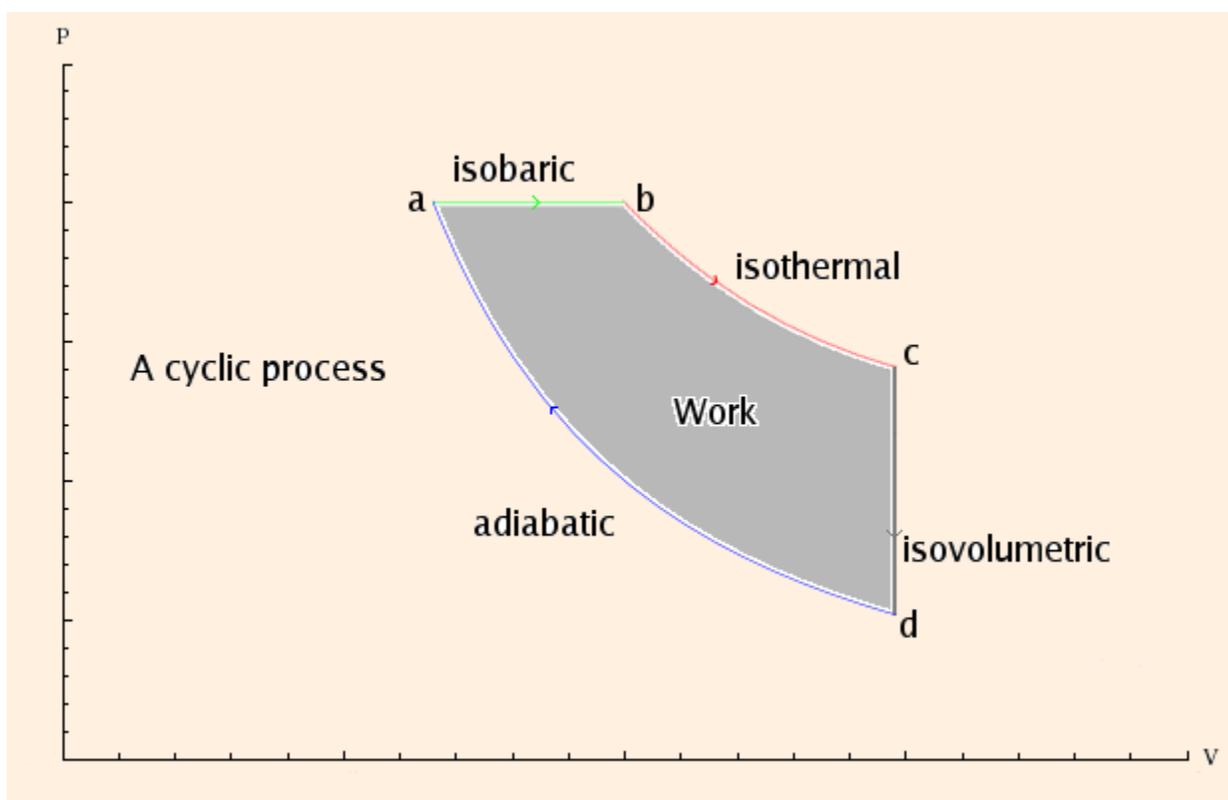
1. Thermodynamic processes can be:

- **isothermal processes**, $\Delta T = 0$ (so $P \sim 1 / V$);
- **isobaric processes**, $\Delta P = 0$ (so $T \sim V$);
- **isovolumetric or isochoric processes**, $\Delta V = 0$ (so $T \sim P$);
- **adiabatic processes**, $\Delta Q = 0$ (so $P \sim 1 / V^\gamma$);
- **cyclic processes**, *all* state variables (P, V, T, E, S) return to their original values after each cycle.

(Throughout, we will assume the processes involve an ideal gas with constant n.)

In a cyclic process, the [state variables](#) all return to their initial values after one cycle.

2. Thermodynamical systems are often described using **PV diagrams**, with pressure plotted on the vertical axis and volume plotted on the horizontal axis. In such a diagram, the area under a curve is easily related to work:



Assuming this PV diagram describes a process involving an [ideal gas](#), we can deduce the following:

as $a \rightarrow b$	$P_a = P_b$	$\Delta E_{a \rightarrow b} = n c_v (T_b - T_a)$	$\Delta Q_{a \rightarrow b} = n c_p (T_b - T_a)$	$W_{a \rightarrow b} = -P_a (V_b - V_a)$
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at b	$T_b = P_b V_b / (n R)$	$T_b > T_a$	$\Delta Q_{a \rightarrow b} > 0$	$W_{a \rightarrow b} < 0$
as b→c	$T_b = T_c$	$\Delta E_{b \rightarrow c} = 0$	$\Delta Q_{b \rightarrow c} = -W_{b \rightarrow c}$	$W_{b \rightarrow c} = -n R$
at c	$T_c = P_c V_c / (n R)$		$\Delta Q_{b \rightarrow c} > 0$	$W_{b \rightarrow c} < 0$
as c→d	$V_c = V_d$	$\Delta E_{c \rightarrow d} = n c_v (T_d - T_c)$	$\Delta Q_{c \rightarrow d} = n c_v (T_d - T_c)$	$W_{c \rightarrow d} = 0$
at d	$T_d = P_d V_d / (n R)$	$T_d < T_c$	$\Delta Q_{c \rightarrow d} < 0$	
as d→a	$P_d V_d^{c_p/c_v} = P_a V_a^{c_p/c_v}$	$\Delta E_{d \rightarrow a} = n c_v (T_a - T_d)$	$\Delta Q_{d \rightarrow a} = 0$	$W_{d \rightarrow a} = n c_v$
at a	$T_a = P_a V_a / (n R)$	$T_a > T_d$		$W_{d \rightarrow a} > 0$

In addition, we know that $\Delta E_{a \rightarrow b} + \Delta E_{c \rightarrow d} + \Delta E_{d \rightarrow a} = 0$, but in this case it only tells us that $T_b = T_c$.

From this we can compute the total heat added during the cycle:

$$n c_p (T_b - T_a) + n R T_b \ln (V_c / V_b)$$

and the total work done by the gas:

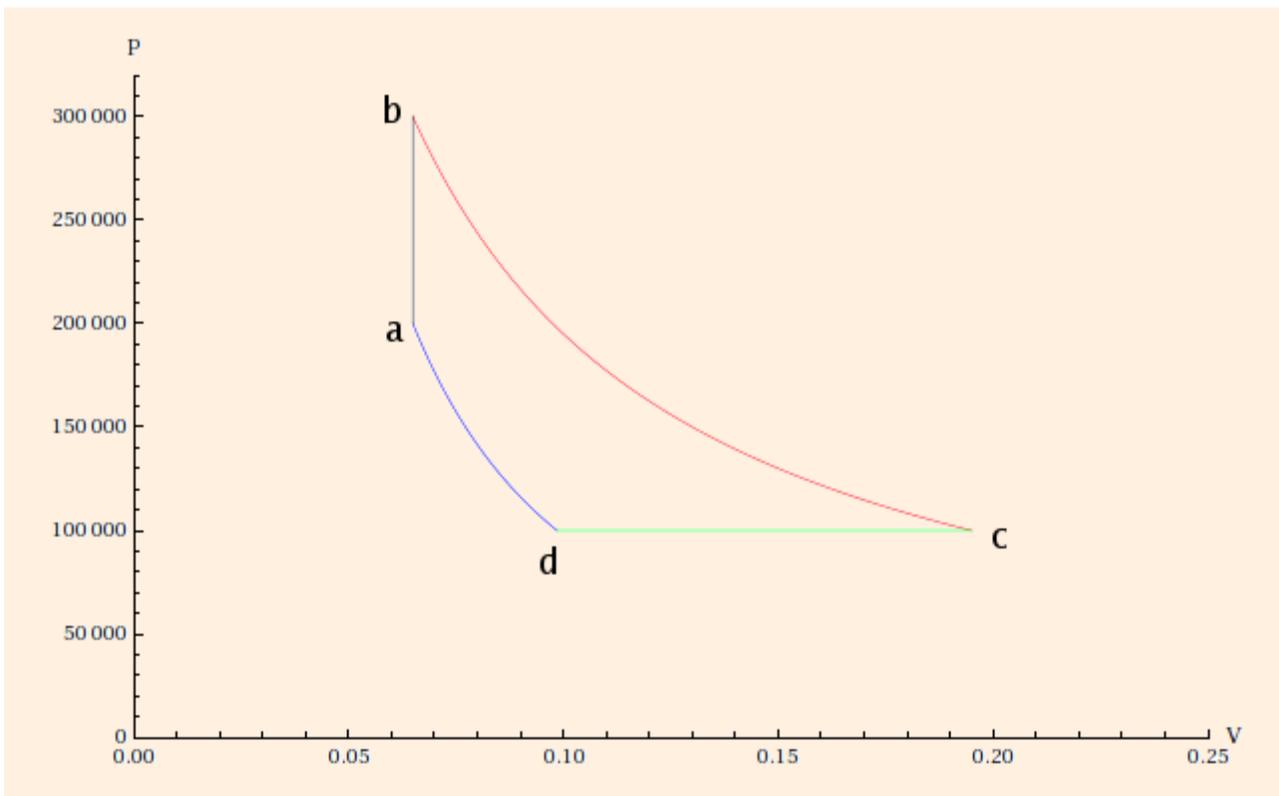
$$P_a (V_b - V_a) + n R T_b \ln (V_c / V_b) - n c_v (T_a - T_d),$$

corresponding to the shaded area in the PV diagram.

Note that heat enters this "engine" in steps a→b and b→c, and exits it in step c→d; the total work done by the engine is positive. If the cycle were operated in reverse, it would be a "refrigerator", taking heat from a cooler environment during step d→c and exhausting it to a warmer environment from c→a; the total work done by the refrigerator is negative.

The meaning of this is that it requires external work to move heat from a cooler to a warmer place.

- To see how this information is applied to a problem, consider the following thermodynamic cycle for $n = 4$ moles of a monatomic ideal gas:



1. from a to b, the system undergoes an isovolumetric increase in pressure;
2. from b to c, the system undergoes an isothermal expansion;
3. from c to d, the system undergoes an isobaric compression;
4. from d to a, the system undergoes an adiabatic compression.

Suppose we are given $P_a = 200,000$ Pa, $P_b = 300,000$ Pa, $P_c = 100,000$ Pa and $V_a = 65$ L.

We know that $P_d = P_c$, $V_b = V_a$, and $T_b = T_c$. We can use the ideal gas law to compute the temperatures at points a and b from the pressure and volumes at those points: 390.907 K and 586.36 K, respectively. From the latter we can compute the volume at point c, which is 195 L.

We can use the [adiabatic equation for an ideal gas](#):

$$P_d V_d^\gamma = P_a V_a^\gamma,$$

to compute $V_d = 98.5216$ L. Finally, we can use the ideal gas law to find that $T_d = 296.252$ K.

Since b to c is an isothermal expansion, the [first law](#) tells us that $\Delta Q_{b \rightarrow c} = -\Delta W_{b \rightarrow c}$. Using the ideal gas law, we find

$$\begin{aligned} \Delta W_{b \rightarrow c} &= - \int_b^c P dV \\ &= - n R T_b \int_b^c dV / V \\ &= - n R T_b \ln (V_c / V_b) = -21,422.9 \text{ J.} \end{aligned}$$

(Note the sign: the gas does external work.)

Using the equations for [isovolumetric and isobaric processes](#), we have

$$\begin{aligned}\Delta Q_{a \rightarrow b} &= n c_v (T_b - T_a) & \Delta Q_{b \rightarrow c} &= n R T_b \ln (V_c / V_b) & \Delta Q_{c \rightarrow d} &= n c_p (T_d - T_c) \\ &= 9750 \text{ J} & &= 21,422.9 \text{ J} & &= -24,119.6 \text{ J}\end{aligned}$$

Finally, consistent with the fact that $\Delta E = 0$ for a cycle, we compute

$$\begin{aligned}\Delta W_{a \rightarrow b} &= 0 & \Delta W_{b \rightarrow c} &= -n R T_b \ln (V_c / V_b) & \Delta W_{c \rightarrow d} &= P_c (V_c - V_d) & \Delta W_{d \rightarrow a} &= c_v (P_a V_a \\ & & &= -21,422.9 \text{ J} & &= 9647.84 \text{ J} & &= 4721\end{aligned}$$

4. The **efficiency** of an engine is

$$\begin{aligned}\varepsilon &= W / Q_h \\ &= (Q_h - Q_c) / Q_h \\ &= 1 - Q_c / Q_h.\end{aligned}$$

Here, energy is taken in as Q_h , work W is done by the engine, and the waste heat is discharged as Q_c .

In the example above, $Q_h = 31,172.9 \text{ J}$, $W = 7053.33 \text{ J}$, $Q_c = 24,119.6 \text{ J}$ and $\varepsilon = 22.6265\%$.

This calculation obscures some interesting facts:

- for this cycle, as the number of [degrees of freedom](#) of the gas $\chi \rightarrow \infty$ (with all other values unchanged), $\varepsilon \rightarrow 0$ as $1/\chi$ (more heat must be removed during isobaric cooling to lower the temperature the same amount, because more of the heat comes from non-translational degrees of freedom which do not affect temperature);
- ε does not depend on n ; increasing n will only lower the temperatures (via the ideal gas law; with more molecules, less energy is available per molecule);
- while the efficiency is a complicated function of the given values, it turns out that, holding all other values constant, increasing P_b or decreasing P_c will increase ε , while the value of V_a does not alter ε at all and the chosen value of P_a is almost optimal.

Of course, for another cycle, the results can be *very* different.

For an air conditioner, **heat pump** in air conditioning mode, or refrigerator, $\varepsilon = Q_{\text{transferred}} / W_{\text{required}}$.

The efficiency of a refrigerator can be greater than 1, since

$$\varepsilon = Q_c / (Q_h - Q_c)$$

$$= 1 / (Q_h / Q_c - 1),$$

where Q_c is the heat removed from the cooler environment and Q_h is the heat exhausted into the warmer environment. Note that Q_h must be greater than Q_c .

5. We often consider a cycle operating between two **heat reservoirs** (of infinite heat capacity), one at temperature $T_{h(\text{ot})}$ and the other at temperature $T_{c(\text{old})}$. For such a device, ΔS includes the engine itself *and* the reservoirs. Since the engine operates in a cycle, its ΔS is 0, so for isothermal transfers,

$$\Delta S = -\Delta Q_h / T_h + \Delta Q_c / T_c.$$

In general, $\Delta S = \int dQ / T$.

For the example above, $\Delta S_{b \rightarrow c} = 36.5355 \text{ J/K}$, and of course $\Delta S_{d \rightarrow a} = 0$. To compute $\Delta S_{a \rightarrow b}$ and $\Delta S_{c \rightarrow d}$, we use the ideal gas law to express T as a function of P and V :

$$\begin{aligned} \Delta S_{a \rightarrow b} &= \int n c_v dT / T \\ &= \int n c_v (V dP / (n R)) / (P V / (n R)) \\ &= n c_v \ln (P_b / P_a) = 20.2262 \text{ J/K} \end{aligned}$$

and

$$\begin{aligned} \Delta S_{c \rightarrow d} &= \int n c_p dT / T \\ &= \int n c_p (P dV / (n R)) / (P V / (n R)) \\ &= n c_p \ln (V_d / V_c) = -56.7617 \text{ J/K} \end{aligned}$$

The changes in entropy of the reservoirs are of course dependent on their temperatures. Assuming that the isobaric compression lost heat to a reservoir at room temperature ($< T_d$), and that the isochoric and isothermal processes gained heat from a reservoir at 320 C ($> T_b$),

$$\Delta S_{\text{cold reservoir}} = 24119.6 / 293.15 \text{ J/K} = 82.277 \text{ J/K} \text{ and}$$

$$\Delta S_{\text{hot reservoir}} = -31172.9 / 593.15 \text{ J/K} = -52.555 \text{ J/K},$$

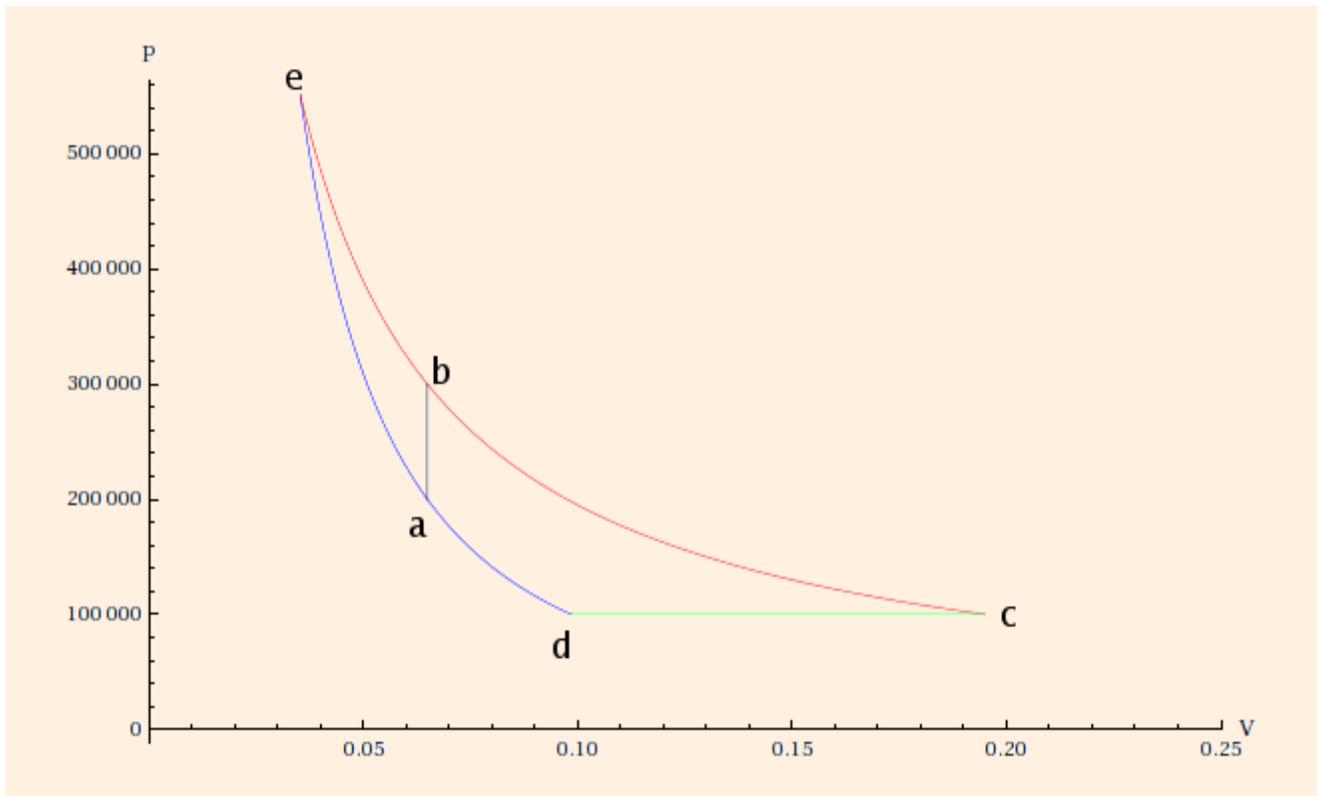
so that

$$\Delta S_{\text{reservoirs}} = 29.722 \text{ J/K},$$

which is greater than zero, as required by the second law of thermodynamics.

If we did not know T as a function of P and V , it would be necessary to connect each pair of endpoints with a combination of adiabatic and isothermal processes, and compute the change in entropy using

those new processes. For example:



Process $a \rightarrow e$ is an adiabatic process, and $e \rightarrow b$ is isothermal. $P_e = 551,135 \text{ Pa}$ and $V_e = 35.3815 \text{ L}$, from

$$\begin{aligned} P_a V_a^\gamma &= P_e V_e^\gamma \\ &= n R T_b V_e^{\gamma-1} \end{aligned}$$

This gives us (using the same equations as above)

$$\Delta Q_{a \rightarrow e} = 0 \text{ and}$$

$$\Delta Q_{e \rightarrow b} = 11,859.9 \text{ J.}$$

Since entropy is a state variable,

$$\Delta S_{a \rightarrow b} = \Delta S_{e \rightarrow b} = 20.2262 \text{ J/K,}$$

as before. Either way, the entropy change *of the engine* is zero, because it is a cycle: all state variables, including entropy, end at the same state in which they began. Therefore $\Delta S_{c \rightarrow d} = -56.7617 \text{ J/K}$.

6. The **Carnot cycle** is the most efficient cyclic thermodynamic process conceivable:

1. isothermal expansion, with $\Delta Q = Q_h$ at T_h ;
2. adiabatic expansion, with $T_h \rightarrow T_c$;

3. isothermal compression, with $\Delta Q = -Q_c$ at T_c ; and
4. adiabatic compression, with $T_c \rightarrow T_h$.

What makes it so is that each step of the Carnot cycle is **reversible**: all changes of state are infinitesimally close to equilibrium.

Reversible changes of state are infinitely long; all real changes of state are irreversible.

In isothermal processes, by definition the gas is in thermal equilibrium with the reservoir. An adiabatic process can be irreversible:

Consider a closed, thermally insulated volume with a partition in the middle, such that nearly all of the gas molecules are on one side of the partition; the other side is a nearly perfect vacuum. With removal of the partition, the gas adiabatically but irreversibly doubles in volume.

A reversible adiabatic process would be a change in volume by infinitesimal steps while the gas is thermally insulated.

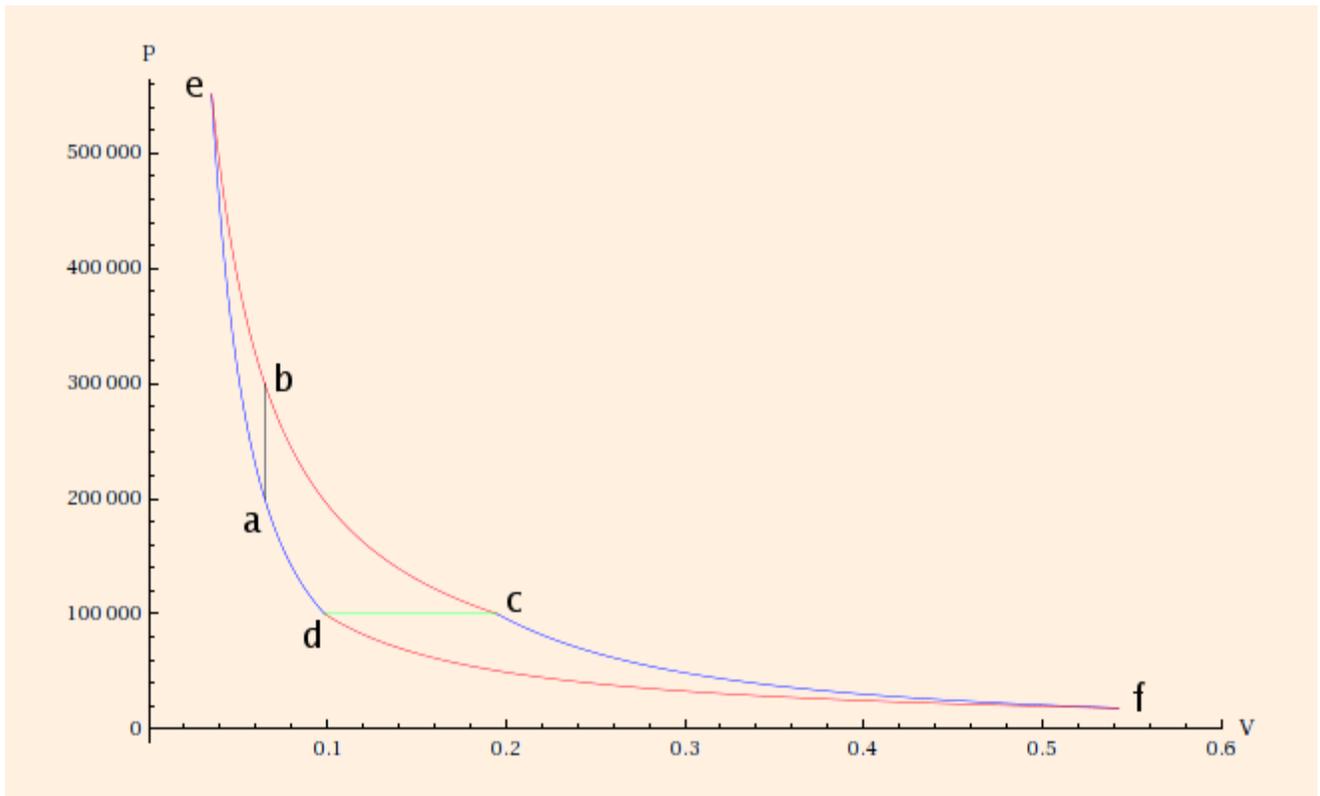
Since it is reversible, the total entropy change of the Carnot cycle reservoirs is zero. This gives us

$$0 = -Q_h / T_h + Q_c / T_c$$

or

$$Q_c / Q_h = T_c / T_h.$$

If we attempt to compute the entropy change for $c \rightarrow d$ by finding a point f on the PV diagram such that $c \rightarrow f$ is adiabatic and $f \rightarrow d$ is isothermal, we find that we have constructed a Carnot cycle:



Hence the total entropy change is zero *including the reservoirs*, and its efficiency is

$$1 - T_d / T_b = 49.4761\%.$$

The efficiency of a Carnot Refrigerator is $T_c / (T_h - T_c)$.

7. Thermodynamic cycles of practical interest include:

- the **Diesel Engine**, consisting of adiabatic compression ($a \rightarrow b$), isobaric heating ($b \rightarrow c$), adiabatic expansion ($c \rightarrow d$) and isovolumetric cooling ($d \rightarrow a$);

$$\varepsilon = 1 - (T_d - T_a) / ((1 + 2 / \chi) (T_c - T_b))$$

- the **Otto Cycle**, consisting of adiabatic compression, isovolumetric heating, adiabatic expansion and isovolumetric cooling;

$$\varepsilon = 1 - (V_{\text{small}} / V_{\text{large}})^{(2 / \chi)}$$

- the **Stirling Engine**, consisting of alternating isothermal and isovolumetric processes.

$$\varepsilon = 1 / (1 + T_{\text{lower}} / (|\Delta T| + \chi / (2 \ln (V_{\text{large}} / V_{\text{small}}))))$$

In each case, ε was computed for an ideal gas. Note that in each case, it is independent of n , and increases with decreasing χ . This generalizes what we saw above: if we think of work as the result of increased temperature, less heat input is required to change the temperature of a gas with fewer degrees of freedom.

8. It is important to remember that these are *models* of real thermodynamic process. In actual physical processes,
- gasses are *never* perfectly ideal;
 - n is *never* constant;
 - *nothing* has infinite heat capacity; and
 - *no* process is perfectly adiabatic (or, of course, reversible).
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